

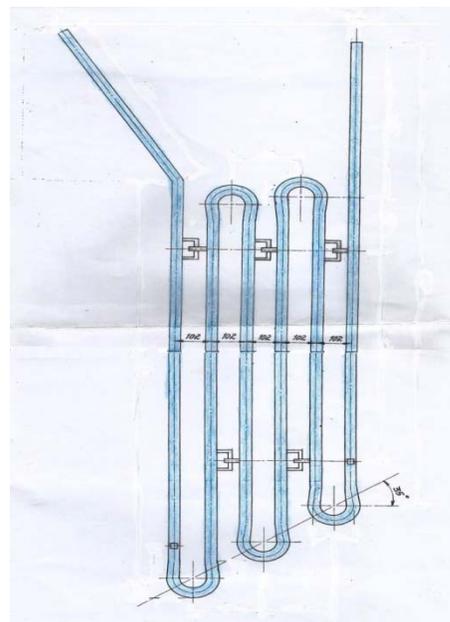
# Enhancing Plant Efficiency by Raising the Degree of Superheat in steam

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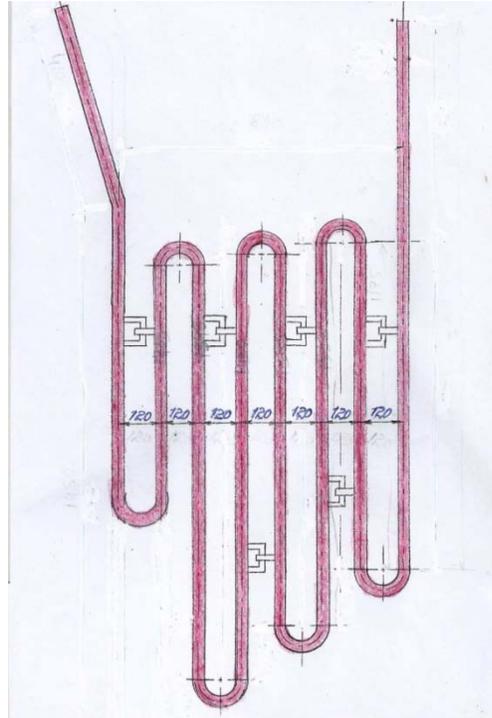
## Advantages of Higher Degree of Super-heat

- More energy will be transported through same amount of steam without modifying the pressure of the boiler.
- Capacity of the Boiler to generate energy with the same overall specifications will enhance.
- Capacity of turbines to convert energy will increase with out any modification in their structure.
- Lesser quantity of steam having higher energy will be required for process use.
- Comparatively smaller size steam handling equipment will be required.

## Original Coil Design



## Modified Coil Design



## Data from Boiler Specifications

- Rated capacity of Boilers (p) = 50Tph.
- Working Pressure @325°C = 24 kg/cm<sup>2</sup>
- Surface area of super-heater. = 76m<sup>2</sup>
- Single coil length = 11m
- No. of super-heater coils. = 58
- Super-heated steam temp. = 325°C
- Temperature of gasses entering into the super-heater. (T1) = 1000°C

## Data from Standard Values

All standard values are taken from Huga's Handbook of cane sugar engineering, Molierer Charts, steam tables other references sited & laboratory analysis

- Specific Heat of gasses (C) = 0.32 kcal/kg/°C
- Mean specific heat of steam (c) = 0.50 kcal/kg°C.
- Moisture in Bagasse (w) = 52.1%

### Data from Standard Values

- Dryness fraction of saturated steam (x) = 0.96.
- Latent heat of vaporization at boiler press. (r) = 440 kcal/kg.
- Temp. of saturated steam at boiler press (t) = 225°C.
- Coefficient of heat transfer (k) = 65 kcal/m<sup>2</sup>/hr/°C
- Coefficient of un-burnt losses ( $\infty$ ) = 0.9.
- Excess air ratio (m) = 1.5

### **Data from Calculated values:**

- **New Specifications:** Super-heated steam temperature-Required (T)=360°C
- **Weight of Bagasse to be burnt (B):**  $B = p/2.1 = 50000/2.1 = 23,809.5$  kg/h

### Data from Calculated values:

- **Mass of Gasses:**

$$\begin{aligned} P_g &= 5.76(1-w) m+1 \\ &= 5.76 (1-0.521) 1.5+1 \\ &= 5.138 \text{ kg/kg of bagasse} \end{aligned}$$

- **Total mass of gasses**

$$\begin{aligned} P &= P_g * B \\ &= 5.138 * 23809.5 \\ &= 122,346 \text{ kg/h} \end{aligned}$$

### Data from Calculated values:

- Quantity of heat transmitted by Super-heater

$$M = \infty * P * C(T_1 - T_2)$$

$$\text{Again } M = p(1-x)r + p * c (T-t)$$

$$\text{Thus } \infty * P * C(T_1 - T_2) = p(1-x)r + p * c (T-t).$$

$$\text{Putting the values in this expression thus gives: } 0.9 * 122346 * 0.32(1000 - T_2)$$

=50000(1-.96)440+50000 \*0.50 (360-225); Finally Temperature of Gasses leaving the super-heater T2=879°C

**Data from Calculated values:**

- Temperature of gases leaving the Super-heater:T2= 879°C.( This calculation has been shown in previous slide).

**Data from Calculated values:**

- Heating Surface of the Super-heater. (S)
- =  $p(1-x)r + p*c(T-t)/[k(T1+T2)/2-(T+t)/2]$
- =  $50000(1-.96)440 + 50000*0.50(360-225) /65[(1000 + 879)/2 - (360 + 225)/2] = 101m^2$ .
- Single coil length = 12.8m.
- No. of coils= 66.
- Tube dia = 38 mm

**BAGASSE SAVING.**

Description	Season	
	2013-14 (After Change)	2012-13 (Before Change)
Cane Crushed	588,138 tons	533,616 tons
Steam % cane	60.5	61.8
Live Steam temp.	355°C	320°C
Energy in live steam	762 kcal/kg	745 kcal/kg
Exhaust Steam temp.	188°C	175°C
Energy in exhaust Steam	688 kcal/kg	681 kcal/kg
Total energy carried by Steam in the season	2.4*10 <sup>11</sup> kcal	2.2*10 <sup>11</sup> kcal

### Bagasse saving.

- After modification of super-heater, a larger amount of energy is carried by a smaller quantity of steam to cater the needs of process house at a higher crushing rate.
- While calculating the bagasse saving, the effect of higher crushing of this season is nullified by considering crushing of 2012-13. Also, same fiber % is considered.

Bagasse consumption @ 60.5% steam on cane=161,418tons. Bagasse consumption @61.8% steam on cane= 164,887tons. Bagasse saving due to higher degree of super-heat=3,469tons.

### Cost of Project

- **Cost of constructing new super-heaters:** = Rs: 4,500,000
- Details

Description	Cost (Rs.)
Tubes + Other Material	1,600,000
Labor Charges	2,700,000
Welding Rods & Cutting Gas	50,000
Masonry, Insulation & Electricity	150,000

### Return on Investment

- Saving in rupees, bagasse @Rs.2500 per ton. = Rs. 8,672,500
- **Return on Investment.** (Considering 160 days season).
  - Pay back =80 days
  - Subsequent saving= Rs 8.5 Million each year

**Thank You**